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# Efficient H<sub>2</sub> production and TN removal for urine disposal using a novel photoelectrocatalytic system of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> - MoNiCuO<sub>x</sub>/Cu

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# ABSTRACT

Urea is considered as the potential hydrogen carrier. However, decomposition of urea to generate hydrogen gas ( $H_2$ ) is severely constrained by sluggish kinetics and the high over-potential of HER. In this study, we propose a novel photoelectriccatalytic (PEC) system of  $Co_3O_4/BiVO_4$  - MoNiCuO<sub>x</sub>/Cu to realize efficiently  $H_2$  production and TN removal in urine treatment. The key design is that an appropriate valence band position of  $BiVO_4$  photoanode, which can generate Cl = Selectively and suppress HO = Extremely, is selected for rapidly converting urea to  $N_2$  instead of  $NO_3$ .  $Co_3O_4$ , as a co-catalyst of photoanode, matches exactly the Fermi level with  $BiVO_4$ , driving the separation and transfer of photogenerated charge of  $BiVO_4$  greatly due to the built-in electric field of p-n heterojunction of  $Co_3O_4/BiVO_4$ . Meanwhile, the yield of Cl = Extremely has been improved by an orders of magnitude compared with Extremely hy Extremely has been improved by an orders of magnitude compared with Extremely hy using Extremely has been improved by an orders of magnitude compared with Extremely hy using Extremely has been improved by in-situ growth of nanowires and the load of Extremely hy using Extremely has prepared by in-situ growth of nanowires and the load of Extremely hy using Extremely hy Extremely hy Extremely hy Extremely hy Extremely hy Extremely hy Extremely has been improved by an order of Extremely has been improved by

## 1. Introduction

Urea (CO(NH<sub>2</sub>)<sub>2</sub>) is widely present in municipal domestic sewage and enriches 80% of nitrogen, in which discharge without effective treatment will cause eutrophication of water bodies [1–3]. Hence, different techniques are developed in the disposal of urine, such as biological technologies, electrochemical means and photochemical methods [1,4,5]. However, urea is the possible source of hydrogen, in which the recovery of hydrogen energy is often omitted [6]. Moreover, compared to water splitting (Eq. 1), H<sub>2</sub> production from urea decomposing has a relatively smaller potential (Eq. 2) [6,7].

$$2 H_2O \rightarrow 2 H_2 + O_2 H^0 = 1.23 \text{ V vs-SHE}$$
 (1)

$$CO(NH_2)_2 + H_2O \rightarrow N_2 + CO_2 + 3 H_2 H^0 = 0.084 \text{ V vs} \cdot \text{SHE}$$
 (2)

Therefore, designing a novel urine treatment system to realize the rapid removal of total nitrogen (TN) and recovery of hydrogen energy is promising. However, the denitrification of urea undergoes the sluggish kinetics because of the occurrence on the surface of catalyst and the peroxidation of nitrate (NO $_3$ ). Interestingly, existing reports and our studies confirm that chlorine free radical (Cl $_{\bullet}$ ) is capable of rapidly converting nitrogen-compounds to N $_2$  instead of NO $_3$  due to its high activity and selectivity [5,8–12]. Hence, a technology for in-situ activation of Cl $_1$  to generate Cl $_{\bullet}$  is designed, which can rationally utilize Cl $_1$  in urine and solve the problem of selective oxidation of urea to N $_2$  and inhibits the production of NO $_3$ . Based on this design concept, how to further efficiently generate Cl $_{\bullet}$  is the essential for urea degradation. Recently, photoelectrocatalysis (PEC) has attracted much attention, which can efficiently generate radicals [1,11,13,14]. Meanwhile, the

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common photoanodes, such as WO<sub>3</sub> and TiO<sub>2</sub> [15-17], have been utilized in PEC systems, but the selectivity towards Clo is relatively lower due to its un-match valence band position [18-22], which is easy to generate hydroxyl radical (HO•) per-oxidizing urea to NO<sub>3</sub> [23]. Undoubtedly, BiVO<sub>4</sub> (narrow band: 2.48 eV) is an alternative visible-light active photoanode due to its appropriate band gap, which can selectively generate Cl• and extremely suppress the generation of HO• [12, 14,24–26]. Besides, Co<sub>3</sub>O<sub>4</sub> (narrow band: 1.81 eV) is another suitable catalyst in valence band position, in which the Fermi level exactly matches BiVO<sub>4</sub> and forms the p-n heterojunction [27-30]. Thereafter, the built-in electric field is formed in the Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> heterojunction, which drives electrons of Co<sub>3</sub>O<sub>4</sub> into the conduction band (CB) of BiVO<sub>4</sub>, promotes the transfer of holes (h<sup>+</sup>) of BiVO<sub>4</sub> to the valence band (VB) of Co<sub>3</sub>O<sub>4</sub>, greatly reduces the recombination of photogenerated charges, and significantly improves the generation of Clo. Above, the constructed Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode can realize the efficient and highly selective generation of Clo, which overcome the slow degradation of urea and release hydrogen energy simultaneously.

On the other hand, the energy barrier (over-potential) of hydrogen evolution reaction (HER) on the cathode also needs to be resolved for efficient H<sub>2</sub> generation [31], in which the over-potential is prevalent in the reaction of hydrogen source decomposition [32]. Notably, platinum (Pt) has the lowest over-potential in the field of HER, but scarcity and high cost still hinder its further development [33]. Therefore, it is the reliable strategy to design the non-noble metal catalyst by referring to the reaction kinetics occurring on the Pt surface. Fortunately, some scholars have found that molybdenum nickel (MoNi) based catalysts have outstanding HER capabilities comparable to Pt [34-37]. Notably, how to expose fully the catalytically MoNi sites is important for HER, which will severely determine the H<sub>2</sub> generation [36]. Critically, our previous studies found that the three-dimensional (3D) porous structure of copper foam with good electrical conductivity, low resistance and large specific surface area is used as the substrate [38-40]. Besides, the construction of one-dimensional (1D) nanowires structures on the surface of copper foam supplies numerous catalytic support, which capable of supporting considerable MoNi catalytic active sites, thereby exposing sufficient catalytic active sites for to lower the energy barrier for HER [23,41,42]. Therefore, we designed a novel 3D catalyst consisting of arrays of highly exposed molybdenum nickel copper alloy oxide (MoNiCuOx) nanowires on copper foam (MoNiCuOx/Cu) to efficiently reduce the over-potential of HER, in which MoNiCuOx nanowires are prepared by in-situ growth of Cu(OH)<sub>2</sub> nanowires on copper foam and load of molybdenum nickel (MoNi) alloy sites on Cu(OH)2 nanowires. The results confirmed the over-potential to attain  $-10 \text{ mA cm}^{-2}$  of MoNiCuO<sub>x</sub>/Cu cathode is 49 mV, which was lower than Pt (119 mV).

Thus, we propose a novel photoelectrocatalytic system combining Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode and MoNiCuO<sub>x</sub>/Cu cathode to realize H<sub>2</sub> production and TN removal simultaneously in the urine treatment. In the anode chamber, the h<sup>+</sup> of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> heterojunction efficiently oxidize Cl- to Cl• and further convert urea to N2 and CO2 with avoiding NO<sub>3</sub> generation under irradiation of visible light, in which TN removal is 3.1 times, 4.6 times and 17.9 times higher than the BiVO<sub>4</sub>, WO<sub>3</sub> and TiO2, respectively. In the cathode chamber, the electrons generated during urea oxidation are transferred to the cathode through the external wire to reduce the H+ on the surface of MoNiCuOx/Cu nanowires. Meanwhile, a large number of MoNi alloy sites with excellent hydrogen evolution properties are widely distributed in the MoNiCuO $_{x}$ / Cu cathode, which greatly reduces the over-potential of HER. Besides, H<sup>+</sup> passes through the proton exchange membrane (PEM) to equilibrate the concentration of H<sup>+</sup> in the dual chamber. Ultimately, an extremely dfficient H<sub>2</sub> generation was obtained, in which it is 2.4 times, 3.5 times and 11.0 times and higher than the BiVO<sub>4</sub>, WO<sub>3</sub> and TiO<sub>2</sub>, respectively. The results show that the urea is rapidly decomposed and H<sub>2</sub> is effectively generated synchronously. This study offers a new insight for urine remediation and recovery of hydrogen energy.

# 2. Experiment section

#### 2.1. Chemicals and materials

All of analytical reagent grade reagents were purchased from Sinopharm Chemical Reagent Co., Ltd., China. Fluorine-doped tin oxide (FTO:  $13~\Omega~cm^{-1}$ ) and copper foam (1 mm thick) were purchased from Nippon Sheet Glass and Suzhou Taili Metal Foam Co., Ltd., China, separately. Ultra-pure Deionized (DI) water was used to prepare the various required solutions. Meanwhile, the urea in simulated urine and actual urine were employed as the targets and diluted to 30 mg N L $^{-1}$ , in which the simulated urine was prepared as initial urine sample described in Table S1[11].

# 2.2. Preparation of electrodes

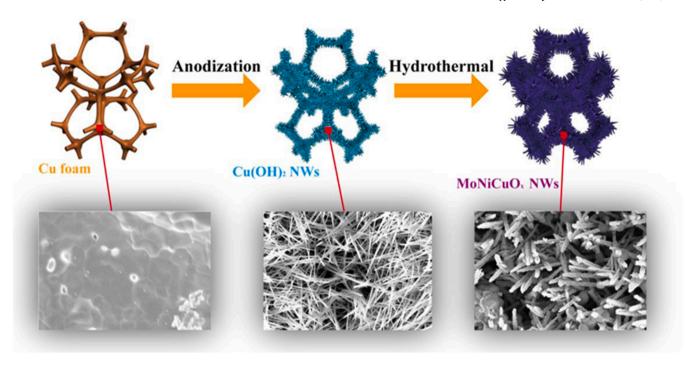
The  $MoNiCuO_x/Cu$  cathode was synthesized by anodization and hydrothermal processes and the detailed was provided in Supplementary material [43,44]: firstly, the smooth copper foam was used anodization process to grow  $Cu(OH)_2$  nanowires, in which dense and slim  $Cu(OH)_2$  nanowires uniformly grown on the surface of the copper foam. Then treated copper foam was consequently treated hydrothermally. Finally, the obtained black  $MoNiCuO_x/Cu$  was vacuum dried overnight, in which  $Cu(OH)_2$  nanowires became rough and uniformly covered with  $MoNiO_x$  alloy (Scheme 1). Additionally, the preparation details of  $Co_3O_4/BiVO_4$  nanorods are shown in the Supplementary material according to pervious works [27,28].

#### 2.3. Experimental setup

The double chamber reactor, assembled from quartz glasses, was equipped for denitrification and hydrogen production (Fig. S1). Meanwhile, the cathode and anode chambers are separated by a proton exchange membrane (PEM), on which  $\rm H^+$  in the anode chamber entered into the cathode chamber through PEM. Moreover,  $\rm Co_3O_4/BiVO_4$ , as the working electrode, was placed in the anode chamber facing the light source; Ag/AgCl, as the reference electrode, was also placed in the anode chamber; MoNiCuO $_x/\rm Cu$ , as the counter electrode, was placed in the cathode chamber parallel to the working electrode. The simulated urine (100 mL), 50 mM Na $_2\rm SO_4$  and 50 mM NaCl were placed in the anode chamber, and the cathode chamber added 50 mM Na $_2\rm SO_4$  as the electrolyte. Additionally, a 350 W xenon lamp (Perfect, China) provided a light intensity of 100 mW cm $^{-2}$  as a simulated solar light source.

# 2.4. Analytical methods

A scanning electron microscope (SEM, Zeiss SUPRA55-VP), X-ray diffractometer (XRD, Rigaku D-Max B), X-ray photo-electron spectroscopy, Ultraviolet photoelectron spectroscopy (XPS, UPS, AXIS UltraDLD) and high-resolution transmission electron microscope (HRTEM) coupled with an X-ray energy dispersive spectrometer (EDS) were used to characterize the different properties of the prepared electrodes, respectively. Besides, the colorimetric method applying with a UV-visible spectrophotometer (752 N, INESA, Shanghai) was used to determine the concentration of active chlorine, nitrate and ammonia. Additionally, TN/TOC analyzer (Analytikjena, Germany) was used to detect TN and TOC. The electron spin resonance method (ESR, Micro ESR, USA) was to detect the free radical species. The high performance liquid chromatography (HPLC-2010 Plus, Shimadzu) was applied to determine the concentration of urea. The generated gases (N2 and H2) were analyzed by on-line GC (Fuli Instruments, 9790Plus, China). Moreover, the detailed and data-processing methods was provided in the Supplementary material.



Scheme 1. Scheme illustration of the fabrication procedures of the MoNiCuO<sub>x</sub>/Cu electrode.

# 3. Results and discussions

# 3.1. Characterization of MoNiCuO<sub>x</sub>/Cu cathode

The MoNiCuO $_x$ /Cu was successfully prepared by two steps (Scheme 1). Fig. 1a and the high-magnification image (Fig. 1b) further showed the specific surface morphology, in which the surface of the MoNiCuO $_x$  nanowires became much more rough. Besides, compared to smooth Cu (OH) $_2$  nanowires, MoNiCuO $_x$  nanowires displayed no obvious change in length while became significantly thicker in diameter. In Fig. S3, the XRD patterns of the copper foam (Cu), Cu(OH) $_2$ /Cu and MoNiCuO $_x$ /Cu were displayed, in which the diffraction peaks at 43.3°, 50.4° and 74.1° originate from the Cu, and the peaks situated at 23.8°, 33.7° and 39.8° are confirmed to Cu(OH) $_2$  [45]. The peaks located at 30.1° and 41.7° are represented to MoNi $_4$ , separately [46]. Besides, the peak situated at 24.5°, 35.7° and 61.0° are indicated MoO $_2$  [44]. Moreover, the peaks

located at  $27.4^{\circ}$  and  $31.0^{\circ}$ , which corresponded to the characteristic diffractions of CuO. These results indicated that MoNi<sub>4</sub> and MoO<sub>2</sub> were effectively covered on the surface of Cu(OH)<sub>2</sub> nanowires. Additionally, the high-resolution transmission electron microscopy (HRTEM) images of the MoNiCuO<sub>x</sub>/Cu was shown in Fig. 1c-d, the lattice fringes with lattice spacing of 0.28 nm was corresponded to the (200) facet of MoNi<sub>4</sub> [44]. Moreover, lattice spacing of 0.35 nm was indicated to the (110) facet of MoO<sub>2</sub> [44]. The results further confirmed the MoNi<sub>4</sub> and MoO<sub>2</sub> were uniformly anchored on Cu(OH)<sub>2</sub> nanowires. Clearly, the TEM-EDX characterizations were signified the nanowire was composed of Cu, Mo, Ni and O elements.

Notably, the detailed chemical composition and element valance states of  $MoNiCuO_x/Cu$  were further provided by X-ray photoelectron spectroscopy (XPS) to further characterize. As shown in Fig. 2a, the prepared  $MoNiCuO_x/Cu$  electrode contained four elements of Mo, Ni, Cu and O, on which the corresponding characteristic peaks appeared in the

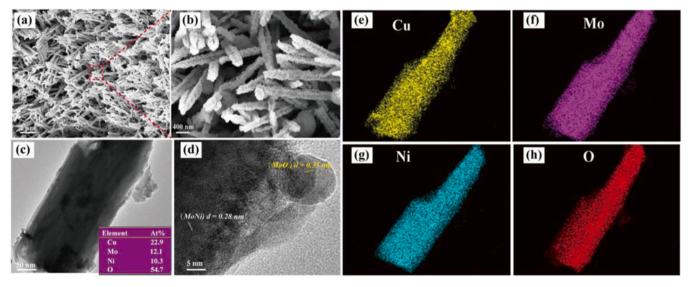


Fig. 1. (a) and (b) SEM images of MoNiCuO<sub>x</sub>/Cu electrode; (c) TEM, (d) HRTEM images and (e-h) EDX mapping images of MoNiCuO<sub>x</sub>/Cu electrode.

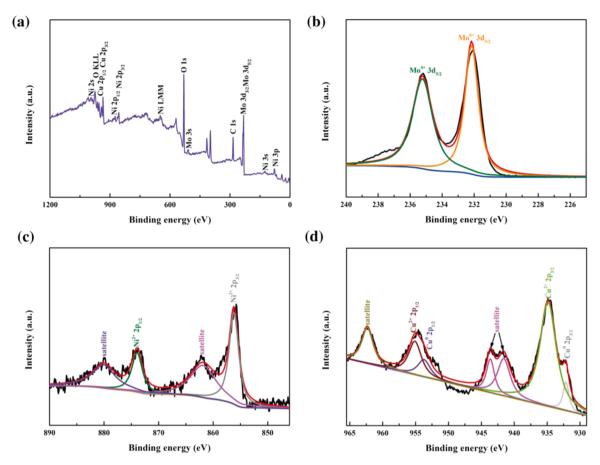


Fig. 2. (a) XPS patterns of (a) MoNiCuO<sub>x</sub>/Cu electrode; (b) Mo 3d peak, (c) Ni 2p peak and (d) Cu 2p peak.

XPS spectrum. Besides, the high resolution spectrum of Mo 3d, Ni 2p and Cu 2p were shown in Fig. 2b-d, respectively. The Mo 3d spectrum can be divided into two high-intensity peaks, which at 235.2 eV (Mo $^{4+}$ ) and 232.2 eV (Mo $^{6+}$ ), separately [36]. In addition, the spectrum of Ni was divided into four peaks. Meanwhile, Ni $^{2+}$  2p $_{3/2}$  and 2p $_{1/3}$  showed the major two peaks with high intensity at 856.2 and 874.0 eV, while the other peaks were the satellites [36]. Additionally, the spectrum of Cu was divided into seven peaks, in which the two high-intensity peaks locating at 934.8 and 955.1 eV were indexed to Cu $^{2+}$  2p $_{3/2}$  and 2p $_{1/2}$ , while the two low-intensity peaks emerging at 932.1 and 953.6 eV were assigned to Cu $^{0}$  2p $_{3/2}$  and 2p $_{1/3}$  [45]. Similarly, the spectrum of Cu appeared the satellites.

After identifying the prepared MoNiCuO<sub>x</sub>/Cu electrode, the hydrogen evolution reaction (HER) performances, as the most important property, was examined by different electrodes. Platinum (Pt) was the most outstanding HER material according to previous studies. Hence, we tested the linear sweep voltammetry (LSV) curves to compare the prepared cathode with Pt. Meanwhile, MoNiCuO<sub>x</sub>/Cu cathode showed the most superior HER performance among all compared Pt and copper foam (Cu), exhibiting the lowest onset over-potential to attain  $-10 \text{ mA cm}^{-2}$ . Significantly, the over-potential of MoNiCuO<sub>x</sub>/Cu was 49 mV, which was much smaller than Cu (346 mV) and Pt (119 mV), respectively. Moreover, the HER performance of MoNiCuO<sub>x</sub>/Cu was the most outstanding than listed in Fig. 3c, of which the specific details are displayed in the Table S2. Meanwhile, the over-potentials of both Cu (OH)<sub>2</sub>/Cu (147 mV) and MoNiO<sub>x</sub>/Cu (103 mV) were smaller than Cu, which confirmed the Cu(OH)<sub>2</sub> catalytic supports and MoNi catalytic sties both could reduce the over-potential of HER[39,44]. Besides, the Tafel slopes sourced from the LSV polarization curves was another key parameter to indicate the reaction kinetics of hydrogen evolution. As shown in Fig. 3b, the Tafel slope of MoNiCuO<sub>x</sub>/Cu cathode was only

75 mV dec<sup>-1</sup> while the Tafel slope of Cu and Pt were 209 mV dec<sup>-1</sup> and 127 mV dec<sup>-1</sup>, which further explaining the most optimal H<sub>2</sub>O adsorption and hydrogen desorption processes. Besides, the Tafel slope was dropped from 209 mV dec<sup>-1</sup> to 75 mV dec<sup>-1</sup> after modified MoNiCuOx nanowires, declaring the both Volmer step and Tafel step had been dramatically accelerated. Therefore, we proposed a possible process for the dissociation of H<sub>2</sub>O molecules in MoNiCuO<sub>v</sub> nanowires (Fig. S4), in which the hydrogen atom of H<sub>2</sub>O molecules was adsorbed and activated on the MoNi<sub>4</sub> active sites. Then, the hydrogen atom was activated to form active hydrogen (H\*), and H\* was desorbed from MoNiCuO<sub>x</sub> nanowires with the catalysis of MoO<sub>2</sub>. Moreover, the density functional theory (DFT) calculations were applied to estimate the adsorption energies and the Gibbs free energy changes for H2O adsorption ( $\Delta G_{H2O}$ ) and  $H_2$  formation ( $\Delta G_{H2}$ ), of which the structures and the calculated energies were displayed in Fig. S5. As shown in Fig. S5e, H<sub>2</sub>O adsorption on the surface of MoNi<sub>4</sub> ( $\Delta G_{H2O} = -0.59$  eV) was much more favorable than  $MoO_2$  ( $\Delta G_{H2O} = -0.25$  eV), but  $MoO_2$ had a small energy barrier for the  $H_2$  formation ( $|\Delta G_{H2}|$ ) (0.09 eV). Conversely, although MoNi<sub>4</sub> had a sluggish process in H<sub>2</sub> formation, the free energy values implied a more favorable H2O adsorption on MoNi4 active sites (Fig. S5f). Thus, the active sites of MoNi<sub>4</sub> and MoO<sub>2</sub> together promoted the HER, which further demonstrated the possible HER reaction on MoNiCuOx nanowires. Besides, electrochemical surface area (ECSA) was calculated from cyclic voltammetry (CV) curves using the principle of electrochemical double layer capacitance, in which the ECSA was 4.9 times higher after modification of MoNiCuO<sub>x</sub> nanowires (Fig. S6), indicating the large specific surface for HER performance. Actually, the excellent properties of ideal MoNiCuO<sub>x</sub>/Cu electrode also need to include stability. Fig. 3d revealed the stabilized over-potential at the current density of  $-10 \text{ mA cm}^{-2}$ , and there was no obvious variation in polarization curve between initial test and after multi-current

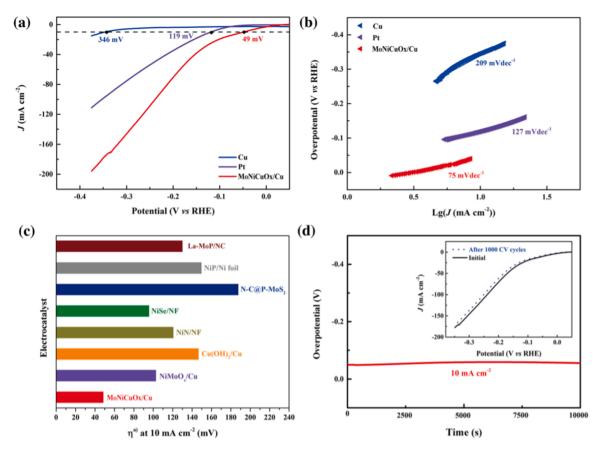


Fig. 3. (a) LSV curves of all compared electrodes tested at 1 M KOH with scanning rate of 10 mV s<sup>-1</sup>; (b) Tafel slopes of contrastive electrodes; (c) Comparison of the current densities at -10 mV among different water alkaline electrodes; (d) Polarization curves of MoNiCuO<sub>x</sub>/Cu electrode at the initial cycle and after 1000 cycles.

stability test, proving its superior durability.

# 3.2. Characterization of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode

In order to confirm the success preparation of  $Co_3O_4/BiVO_4$ , FE-SEM was used to characterize the morphology of  $BiVO_4$  and  $Co_3O_4/BiVO_4$ . In Fig. S7a-b, the appearance of  $Co_3O_4/BiVO_4$  exhibited no obvious difference after the loading of  $Co_3O_4$ . However, it could be found that the surface of the nano-pillared  $BiVO_4$  became rough and appeared some particles at higher magnification, which were the anchored  $Co_3O_4$  [27]. Moreover, in the cross-sectional images (Fig. S8), the thickness of  $BiVO_4$  film was 1.58  $\mu$ m while the thickness of film was increased to 1.71  $\mu$ m after the modification of  $Co_3O_4$ . Besides, the EDS results (Fig. S6c-f) further confirmed the  $Co_3O_4$ .

Additionally, the XRD pattern was utilized to further characterize success preparation of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub>. As shown in Fig. S8a, XRD patterns of BiVO<sub>4</sub> and Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> appeared the similar peaks located at 30.5°, 33.6°,34.6°, 35.1° and 37.7°, which corresponded to the characteristic diffractions of BiVO<sub>4</sub> [28]. Moreover, there was a peak located at 37.3° on XRD pattern Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub>, which was characteristic peak of Co<sub>3</sub>O<sub>4</sub> [47]. Besides, XPS spectra was applied to survey the chemical composition and valence state of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> and the results were displayed in Fig. S8b-e. Meanwhile, four characteristic peaks corresponded to the elements of Bi, V, Co and O appeared in the XPS spectrum in Fig. S8b. The high resolution spectrum of Bi 4 f, V 2p and Co 2p were shown in Fig. S8c-e, respectively. Specifically, the characteristic peaks which binding energies located at 797.3 and 781.3 eV can be assigned to the splitting orbital of Co  $2p_{1/2}$  and Co  $2p_{3/2}$ , and the other existence of peaks located at 803.6 and 785.7 eV were the satellites of Co [27]. Based on the above results, there was a strong proof of successful preparation of

## Co<sub>2</sub>O<sub>4</sub>/BiVO<sub>4</sub>

To better characterize the performance of the Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode, LSV curves and electrochemical impedance spectroscopy (EIS) spectra were measured. As shown in Fig. 4a, the photocurrent density of WO<sub>3</sub> and TiO<sub>2</sub> (conventional semiconductors) are 1.31 and 0.08 mA cm<sup>-2</sup> at 1.36 V (vs. RHE), respectively. Correspondingly, the photocurrent density of BiVO<sub>4</sub> was 1.33 mA cm<sup>-2</sup> at 1.36 V (vs. RHE) while increased to 2.26 mA cm<sup>-2</sup> after fabricating the Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> p-n heterojunction, of which the built-in electric field (the space charge layer with opposite charge) can be formed on the interface between p-Co<sub>3</sub>O<sub>4</sub> and n-BiVO<sub>4</sub>. Moreover, the applied-bias photon-to-current metric (ABPC) of BiVO<sub>4</sub> and Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> were estimated (Fig. S10). Meanwhile, the value of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> is 0.33%, which is almost 2 times of bare BiVO<sub>4</sub>, further revealing that p-n heterojunction possesses stronger catalytic activity in the PEC system. The reason was that the built-in electric field can drive photogenerated electrons of p-Co<sub>3</sub>O<sub>4</sub> into the conduction band (CB) of n-BiVO<sub>4</sub> and facilitate the valence band transfer of photogenerated holes (h<sup>+</sup>) in n-BiVO<sub>4</sub> to p-Co<sub>3</sub>O<sub>4</sub>, thereby greatly reducing the recombination of the photogenerated charges of BiVO<sub>4</sub> and Co<sub>3</sub>O<sub>4</sub>, and greatly increasing the photocurrent [29]. Besides, the EIS Nyquist analysis of BiVO<sub>4</sub> and Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> were conducted, in which the diameter of the fitted semicircle represents the charge transfer resistance, inversely to the rate of charge transfer the electrode. Meanwhile, the Nyquist plot of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> was much narrower semicircle diameter than BiVO<sub>4</sub>, which indicated the resistance of BiVO<sub>4</sub> was dramatically decreased after forming the Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> p-n heterojunction (Fig. 4b).

# 3.3. Urea removal and hydrogen generation

The improvement of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> for denitrification and H<sub>2</sub>

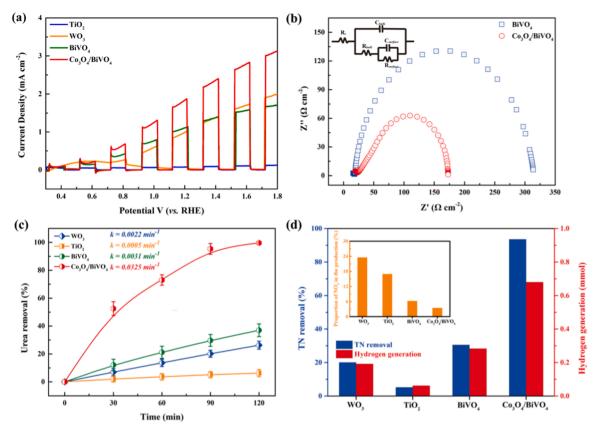


Fig. 4. (a) J-V curves of different electrodes (electrolyte: 0.5 M NaCl, scan rate: 10 mV s<sup>-1</sup>); (b) electrochemical impedance spectroscopy (EIS) analysis of BiVO<sub>4</sub> and Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub>; (c) urea removal versus time by different electrodes; (d) TN removal, hydrogen generation and the proportion of nitrate in the product by different electrodes.

production was well shown in Fig. 4c-d. Meanwhile, Fig. 4c displayed the urea removal via WO<sub>3</sub>, TiO<sub>2</sub>, BiVO<sub>4</sub> and Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub>, of which the removal rate was obeyed the first-order kinetics. Obviously, urea removal in 120 min via Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> (99.5%) was much better than WO<sub>3</sub> (26.3%), TiO<sub>2</sub> (6.3%) and BiVO<sub>4</sub> (37.0%), in which the rate constant of  $Co_3O_4/BiVO_4$  (0.0325 min<sup>-1</sup>) was 14.8 times, 65.0 times and 10.5 times higher than that of  $WO_3$  (0.0022 min<sup>-1</sup>),  $TiO_2$  $(0.0005 \,\mathrm{min^{-1}})$  and BiVO<sub>4</sub>  $(0.0031 \,\mathrm{min^{-1}})$ , respectively. Besides, Fig. 4d showed the TN removal and H<sub>2</sub> generation by WO<sub>3</sub>, TiO<sub>2</sub>, BiVO<sub>4</sub> and Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> via the photoelectrocatalytic treatment. Similarly, Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode showed the best performance on TN removal and H2 production, in which 93.6% of TN was removed and 0.68 mmol H<sub>2</sub> was generated on the MoNiCuO<sub>x</sub>/Cu cathode correspondingly. Meanwhile, TN removal via Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> was 3.1 times, 4.8 times and 17.9 times higher than BiVO<sub>4</sub>, WO<sub>3</sub> and TiO<sub>2</sub>, respectively; Correspondingly, H2 generation via Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> was 2.4 times, 3.5 times and 11.0 times higher than BiVO<sub>4</sub>, WO<sub>3</sub> and TiO<sub>2</sub>, respectively. Markedly, the by-product (NO<sub>3</sub>) was significantly suppressed, which was only 3.5% of urea was peroxidation. That was because the formed pn heterojunction suppresses holes and electrons, which not only strengthened the ability of the photoanode to activate Cl<sup>-</sup> oxidizing urea, but also facilitated the transfer of electrons in the conduction band (CB) to the MoNiCuO<sub>x</sub>/Cu cathode for H<sub>2</sub> production [48,49]. Therefore, the performance on WO3, TiO2 and BiVO4 of TN removal and hydrogen production were all lower than that of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode. Hence, Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode showed the better performance.

# 3.4. Reaction mechanism

The Tauc plot and UPS spectra were applied to verify the band gap and valence band regions of  $BiVO_4$  and  $Co_3O_4.$  The detailed results were

appended in Fig. S11, which take the band gap of 2.48 eV into account, the  $V_{BM}$  and  $C_{BM}$  of BiVO4 were 2.53 and 0.05 V vs. RHE. Likewise, 1.43  $(V_{BM})$  and -0.38  $(C_{BM})$  V vs. RHE for  $Co_3O_4$  (Table S3). Generally, the feasibility of urea removal and hydrogen generation were well demonstrated in Fig. 5 [24,50-52]. Firstly, because of the strong light responsiveness of p-n heterojunction, h<sup>+</sup> and electrons were easily produced on Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode under illumination (Eq. 3). Meanwhile, the electrons in the CB of Co<sub>3</sub>O<sub>4</sub> flowed into the CB of BiVO<sub>4</sub>, then transferred into the MoNiCuO<sub>x</sub>/Cu cathode. Simultaneously, MoNiCuO<sub>x</sub>/Cu cathode with large specific surface and multiple of MoNi<sub>4</sub> active sites can effectively adsorb H<sub>2</sub>O in solution to form H\* (Eq. 4). Next, the other distributed MoO<sub>2</sub> active sites were able to bind H\* to form H<sub>2</sub> and desorb from the cathode surface (Eq. 5). On the other hand, h<sup>+</sup> were produced in both BiVO<sub>4</sub> and Co<sub>3</sub>O<sub>4</sub>, in which the h<sup>+</sup> of BiVO<sub>4</sub> flowed into the valence band (VB) of Co<sub>3</sub>O<sub>4</sub>. The generated h<sup>+</sup> availably oxidized Cl<sup>-</sup> to convert active chlorine (Cl• and Cl<sub>2</sub>) (EqS. 6-7). Thereafter, urea was oxidized to N<sub>2</sub> and CO<sub>2</sub> after a series of reactions by active chlorine (Eqs. 8-9). Furthermore, the concentration of different nitrogen-containing compounds are measured (Fig. S12), in which most of urea was constantly converted to N2 and little part of urea was over-oxidized into NO3. Critically, due to the thermodynamic decomposition of urea is much lower than water splitting (Eqs. 1-2), we compared the current density, in which the current density of decomposition of urea (4.2 mA cm<sup>-2</sup>) was much higher than water splitting (2.5 mA cm<sup>-2</sup>) (Fig. S13). Besides, the energy consumption and cost were calculated and the results were shown in Table S4. Meanwhile, the consumption and cost of urine treatment were 1.18 kWh m<sup>-3</sup> and 0.094  $$\ m^{-3}$$  respectively, which were lower than splitting water (1.73 kWh  $m^{-3}$  and 0.138 \$  $m^{-3}$ ) to produce the same amount of  $H_2$ . Notably, the proposed PEC system can not only treat the urine wastewater but also produce more H2 with the lower cost. Finally, both denitrification and

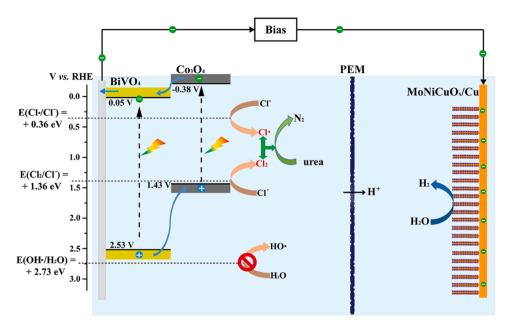


Fig. 5. Illustration of the TN removal and hydrogen generation mechanism in the photoelectrocatalytic system induced by  $Co_3O_4/BiVO_4$  photoanode and MoNiCuO<sub>x</sub>/Cu cathode.

hydrogen energy recovery were realized. Besides, the concentration of active chlorine was detected during the reaction. As shown in Fig. S14a, the active chlorine concentration was constantly increased as the reaction progressed, in which Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> photoanode showed the best capacity of chlorine evolution reaction (CER) and generated 4.45 mg/L of active chlorine in 120 min. Moreover, the electron spin-resonance spectroscopy (ESR) analysis was applied to analyze the radical species in the reaction. Notably, the results of the ESR analysis were explained there were no HO• generated during the reaction. Furthermore, the oxidation of DMPO to DPMOX with active chlorine consisting of Clo and Cl<sub>2</sub> (Fig. S14b) [52,53], which confirmed the urea removal process in Fig. 5. Additionally, benzoic acid (BA) was used probe the Clo, in which BA only reacted with Clo [54] but did not react with Cl2. Besides, nitrobenzene (NB) only reacts with HOo, which eliminated possible interference of HO. As shown in Fig. S14c, the removal of urea was dramatically decreased to 22.6% with the addition of BA while the removal of urea did not change obviously after adding NB, which further confirmed that Cl. was the main oxidant for urea degradation. Markedly, the concentrations of Clo under different anode catalysis were detected and found the concentration of Cl  $\bullet$  generated by Co $_3\mathrm{O}_4/\mathrm{BiVO}_4$  $(1.38\times\ 10^{-7}\ \text{M})$  was extremely strikingly higher than that of  $WO_3$  $(3.11 \times 10^{-9} \text{ M})$ , TiO<sub>2</sub>  $(1.01 \times 10^{-11} \text{ M})$  and BiVO<sub>4</sub>  $(1.30 \times 10^{-8} \text{ M})$ photoanodes (Fig. S14d), which confirmed the superior ability of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> to generate Cl•.

$$Co3O4/BiVO4 + h\nu \rightarrow h^{+} + e$$
 (3)

$$H_2O \xrightarrow{MoNi4} H * + OH^-$$
 (4)

$$2H * \xrightarrow{MoO2} H_2$$
 (5)

$$Cl^- + h^+ \rightarrow Cl \bullet$$
 (6)

$$2Cl^{-} + 2h^{+} \rightarrow Cl_{2} \tag{7}$$

$$CO(NH_2)_2 + 6Cl \bullet + H_2O \rightarrow N_2 + CO_2 + 6Cl^- + 6H^+ \text{ (major)}$$
 (8)

$$CO(NH_2)_2 + 3Cl_2 + H_2O \rightarrow N_2 + CO_2 + 6Cl^2 + 6H^+ (minor)$$
 (9)

# 3.5. The effect of applied potential

The applied potential (vs. RHE) will significantly affect the performance of PEC system, in which the oxidative-capacity of the anode improved with the increase of applied potential. Hence, different applied potential was tested for PEC system research. In Fig. 6a, the removal rate of urea was increased with the increase of the applied potential. Meanwhile, 59.4%, 96.4%, 99.6% and 99.9% of urea were removed at 1.4 V. 1.6 V. 1.8 V and 2.0 V, respectively, which all obeyed the first-order kinetics. Similarly, the total organic carbon (TOC) removal and H<sub>2</sub> generated yield were also increased with the increase of the applied potential. However, the TN removal rate peaked at an applied potential of 1.8 V, in which 93.6% of TN was removed. With further research, it was found that urea would be per-oxidized to NO<sub>3</sub>, and with the increase of the operating potential, the oxidative-capacity of the anode was continuously enhanced, resulting in more NO<sub>3</sub> produced by urea peroxidation (Fig. S15a). Therefore, TN removal had instead declined when the applied potential was 2.0 V. Besides, considering about high applied potential requires more electric energy, the faradaic efficiency (FE) was used to determine the optimal applied potential. The applied potential of 1.8 V was the highest although all of the FE in different applied potentials were relatively low (Fig. S16). That is because the oxidation of urea is accomplished by Clo, in which Clo was not completely reacted with urea and part remained in the solution, resulting in lower FE. If the concentration of urea is increased to enhance the reaction with Clo, the FE also increases simultaneously. To achieve the highest TN removal, the applied potential of 1.8 V was chosen for the PEC system.

# 3.6. The effect of initial Cl concentration

As mentioned, the urea removal was achieved by oxidative conversion of Cl•. Thereafter, the effect of different initial concentrations of Cl were tested, which different concentration of Cl added into the simulated urine. As shown in Figs. 6c, 25.7% of urea was removed when no Cl were added, which may be the h<sup>+</sup> generated on the surface of Co<sub>3</sub>O<sub>4</sub>/BiVO<sub>4</sub> directly oxidized the urea. Obviously, the direct oxidation on the surface of catalyst resulted in very low removal efficiency (0.0024 min<sup>-1</sup>). Conversely, with the introduction of Cl (25 mM), the removal efficiency was significantly improved, which reached

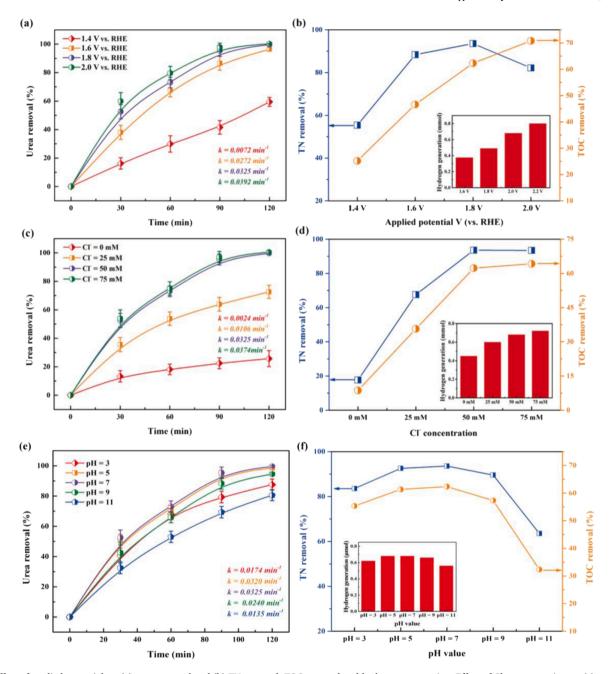


Fig. 6. Effect of applied potential on (a) urea removal and (b) TN removal, TOC removal and hydrogen generation; Effect of Cl<sup>-</sup> concentration on (c) urea removal and (d) TN removal, TOC removal and hydrogen generation; Effect of pH value on (e) urea removal and (f) TN removal, TOC removal and hydrogen generation.

 $0.0106~\text{min}^{-1}$ . When the Cl<sup>-</sup> concentration was further increased to 50 mM, the removal rate of urea was further improved  $(0.0325~\text{min}^{-1})$ . The ability of urea oxidation reached the peak due to the h<sup>+</sup> can activate Cl was limited. Certainly, the removal effect of urea showed no obvious improvement by increasing the Cl<sup>-</sup> concentration (75 mM). Correspondingly, TOC removal, TN removal and  $H_2$  generated yield were also continuously increased with the increase of the Cl<sup>-</sup> concentration (Fig. 6d). Critically, the concentration of NO $_3$  produced by peroxidation decreased with the increase of Cl<sup>-</sup> concentration (Fig. S15b). Therefore, the suitable Cl<sup>-</sup> concentration was 50 Mm.

# 3.7. The effect of pH value

As described above, the thermodynamically favorable product of urea oxidation by  $Cl \bullet$  is  $N_2$ . However, pH value is the key factors for the generation of  $Cl \bullet$ . Therefore, the effects of pH value on the PEC

performance was investigated. In Fig. 6e and Fig. 6f, the good performance occurred under weakly acidic and neutral conditions (pH = 5 and 7), which showed the very similar yield of hydrogen generation and the removal of urea, TN and TOC. However, there was an obvious downward trend when the pH value keeps rising, of which the removal rate of urea was decreased to  $0.0135 \,\mathrm{min}^{-1}$  at pH = 11. Correspondingly, among TOC removal, TN removal and H2 generated yield were also continuously dropped (Fig. 6f). Cl. was unstable existed under alkaline conditions, resulting in the dropping in oxidation of urea [54]. Additionally, 17.1% (5.14 ppm) of  $NO_3$  was generated when pH = 11, in which the selectivity of N<sub>2</sub> was extremely inhibited (Fig. S15c). On the other hand, as Co<sub>3</sub>O<sub>4</sub> could be corroded under strong acid conditions [55], PEC performance, including the removal of urea, TN and TOC, as well as hydrogen production, will slightly decrease when pH= 3. Hence, the constructed PEC system showed superior performance under both weak acidic and neutral conditions.

#### 3.8. Environmental implications

To further clarify the implications of the prepared PEC system, actual urine, as the targets, was employed to examine the practical application value. As shown in Fig. S17, TN of actual urine was removed 95.4% and 2.30 mmol of H<sub>2</sub> was produced simultaneously after 8 h, which maintained the high activity in a complex water matrix. Additionally, there were no obvious change in the micro-structure of the electrodes after urine-treatment (Fig. S18), and the removal of TN and H2 generation were maintained at 92.3% and 0.59 mmol respectively after 5 consecutive runs (Fig. S19), which conformed the robust stability of the PEC system. More importantly, the produced hydrogen energy, as the environmentally friendly energy, is crucial for its practical industrial application. Overall, this PEC system can realize the urine transformation and hydrogen energy recovery, which meets the low-carbon requirements and realize the zero-carbon emission. Hence, the novel PEC technique has the great scientific and economic significance in environmental field.

#### 4. Conclusion

This study proposed a novel dual-chamber PEC system, which constructed with  $\text{Co}_3\text{O}_4/\text{BiVO}_4$  photoanode and  $\text{MoNiCuO}_x/\text{Cu}$  cathode to achieve effective TN removal and simultaneous recovery of hydrogen energy in urine treatment. Meanwhile,  $\text{Co}_3\text{O}_4/\text{BiVO}_4$  photoanode converted  $\text{Cl}^-$  to  $\text{Cl}\bullet$  with high selectivity for efficient TN removal, and  $\text{MoNiCuO}_x/\text{Cu}$  showed the much lower over-potential of HER (49 mV). Both TN removal and  $\text{H}_2$  generation via PEC system were significantly improved. Additionally, PEC system showed good stability during cycling experiments, and also exhibited the similar performance for actual urine treatment. Critically, the cost of urea treatment was only 0.094 \$ m^{-3}\$ and producing 0.68 mmol  $\text{H}_2$ . This study provides a new insight for the possible application of photoelectrocatalytic treatment for urine wastewater.

# CRediT authorship contribution statement

Changhui Zhou: Conceptualization, Data curation, Writing – original draft, Writing – review & editing. Jinhua Li: Visualization, Investigation, Supervision. Jiachen Wang: Investigation, Data curation. Yan Zhang: Investigation, Data curation, Methodology. Lei Li: Methodology. Tingsheng Zhou: Methodology. Chaoyue Xie: Data curation. Jing Bai: Visualization, Supervision. Hong Zhu: Supervision. Baoxue Zhou: Conceptualization, Supervision, Project administration, Writing – review & editing.

# **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

# **Data Availability**

Data will be made available on request.

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# Appendix A. Supporting information

Supplementary data associated with this article can be found in the

online version at doi:10.1016/j.apcatb.2022.122229.

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